

Problema y sistema

Para su tratamiento en una planta, 20500 kg.hr⁻¹ de una salmuera de NaCl al 15% debe ser calentada desde 10°C a 40°C por intercambio de calor con una corriente de agua, la que será enfriada desde los 80°C hasta 45°C. Dimensionar un STHE 1-2 (TEMA: arreglo triangular) Se dispone de tubos 6 m, 3/4" y 1" BWG 14, Acero SS (conductividad térmica: 16.27 W.m⁻¹.°C⁻¹), por los que circula la salmuera. Asumir: que los factores de ensuciamiento son de 0.0005 m².°C.W⁻¹ y 0.0001 m².°C.W⁻¹ para los fluidos que circulan por los tubos y el shell respectivamente; que el costo de un STHE cumple con la siguiente ecuación CSHTE=1000Areq0.8 *um* (*um*: unidad monetaria); un interés anual del 3%; que el costo de energía de bombeo es de 0.15 *um*.kWh⁻¹; que la planta funciona 335 días al año. Puede despreciarse el efecto de la temperatura de pared. Dimensione comparativamente con los métodos de Kern y Delaware. Efectúe un análisis de sensibilidad al modificar el espaciado de los baffles, 0.2, 0.4, 0.6, 0.8 del diámetro de shell y corte de deflectores 0.15, 0.20, 0.25 y 0.30 del diámetro de shell.

DATOS

$$Q_{ms} := 20500 \frac{\text{kg}}{\text{hr}}$$

$$ws := 0.15$$

$$Temp_{Cin} := 10 \quad Temp_{Cout} := 40$$

Intercambiador de coraza y tubo 1:2 (1 paso por coraza, 2 por tubo)
Arreglo triangular
tubos BWG 14 ACERO SS (inoxidable)
Por tubos salmuera, coraza agua
fluido de servicio: agua
fluido de trabajo: salmuera

$$Temp_{Hin} := 80 \quad Temp_{Hout} := 45$$

$$L_t := 6 \text{ m} \quad L_h := 2 \cdot L_t = 12 \text{ m} \quad \epsilon := 2 \cdot 10^{-6} \text{ m}$$

$$\text{tubo 1} \quad D_{in1} := \frac{3}{4} \text{ in} - 2 \cdot 2.11 \text{ mm} = 0.584 \text{ in} \quad D_{o1} := \frac{3}{4} \text{ in} = 0.75 \text{ in}$$

$$\text{tubo 2} \quad D_{o2} := 1 \text{ in} = 0.025 \text{ m}$$

$$D_{in2} := 1 \text{ in} - 2 \cdot 2.11 \text{ mm} = 0.834 \text{ in}$$

$$P_{T2} := 1.25 \cdot D_{o2} =$$

$$k_{ac} := 16.27 \frac{\text{W}}{\text{m} \cdot \Delta^\circ\text{C}} \quad R_{ad} := \left(0.0005 \frac{\text{m}^2 \cdot \Delta^\circ\text{C}}{\text{W}} + 0.0001 \frac{\text{m}^2 \cdot \Delta^\circ\text{C}}{\text{W}} \right)$$

$$\text{n}^\circ \text{ de pasos por tubos } n_{di}$$

$$n_{ms} := 2$$

$$n_{sh} := 1$$

DESARROLLO

INCISO A método de Kern- dimensionamiento

ecuaciones

$$\delta_w(Temp) := \frac{999.83952 + 16.945176 \cdot (Temp) - 7.9870401 \cdot 10^{-3} \cdot (Temp)^2 - 46.170461 \cdot 10^{-6} \cdot (Temp)^3}{1 + 16.87950 \cdot 10^{-3} \cdot (Temp)}$$

$$B(Temp) := \frac{1.3272 \cdot (20 - Temp) - 0.001053 \cdot (Temp - 20)^2}{Temp + 105}$$

$$\mu_w(Temp) := 1.002 \cdot 10^{-3} \cdot 10^{B(Temp)} \cdot Pa \cdot s$$

$$C_1 := \frac{276370}{18.0153} = 1.534 \cdot 10^4 \quad C_2 := \frac{-2090.1}{18.0153} = -116.018 \quad C_3 := \frac{8.125}{18.0153} = 0.451$$

$$C_4 := \frac{-0.014116}{18.0153} = -7.836 \cdot 10^{-4} \quad C_5 := \frac{9.3701 \cdot 10^{-6}}{18.0153} = 5.201 \cdot 10^{-7}$$

$$cP_w(Temp) := (C_1 + C_2 \cdot Temp + C_3 \cdot Temp^2 + C_4 \cdot Temp^3 + C_5 \cdot Temp^4) \frac{J}{kg \cdot \Delta^\circ C}$$

$$C_1 := -0.432 \quad C_2 := 0.0057255 \quad C_3 := -0.000008078 \quad C_4 := 1.861 \cdot 10^{-9} \quad C_5 := 0$$

$$k_w(Temp) := (C_1 + C_2 \cdot Temp + C_3 \cdot Temp^2 + C_4 \cdot Temp^3 + C_5 \cdot Temp^4) \frac{W}{m \cdot \Delta^\circ C}$$

$$C_0 := -0.003241 \quad C_1 := 0.063635 \quad C_2 := 1.013714 \quad C_3 := 0.014595 \quad C_4 := 3317.349$$

$$\delta_{ap}(ws, Temp) := \frac{(ws \cdot C_0 + C_1) \cdot e^{(1 \cdot 10^{-6} \cdot (Temp + C_4)^2)}}{(ws + C_2 + Temp \cdot C_3)} \cdot \left(\frac{kg}{m^3} \right)$$

$$\delta_{sol}(ws, \delta_{ap}, Temp) := \left(\left(\frac{ws}{\delta_{ap}(ws, Temp)} \right) + \frac{(1 - ws)}{\delta_w(Temp)} \right)^{-1}$$

$$V_1 := 16.221789 \quad V_2 := 1.322931 \quad V_3 := 1.484860 \quad V_4 := 0.007469 \quad V_5 := 30.780201 \quad V_6 :=$$

$$\mu_{ap}(ws, Temp) := \frac{e^{\left(\frac{V_1 \cdot ws^{V_2} + V_3}{Temp \cdot V_4 + 1}\right)}}{(V_5 \cdot ws^{V_6} + 1)}$$

$$\mu_{sol}(ws, Temp) := \mu_{ap}(ws, Temp)^{ws} \cdot \left(\mu_w(Temp) \cdot 1000 \frac{m \cdot s}{kg}\right)^{(1-ws)} \cdot 10^{-3} \frac{kg}{m \cdot s}$$

$$a_1 := -0.06936 \quad a_2 := -0.07821 \quad a_3 := 3.847985 \quad a_4 := -11.2762 \quad a_5 := 8.731877 \quad a_6 := 1.8124$$

$$\alpha(ws, Temp) := a_2 \cdot Temp + a_3 \cdot e^{(0.01 \cdot Temp)} + a_4 \cdot ws$$

$$cPi(Temp, ws) := \left(a_1 \cdot e^{(\alpha(ws, Temp))} + a_5 \cdot ws^{a_6}\right) \frac{J}{kg \cdot \Delta^\circ C}$$

$$cPsol(Temp, ws) := (1-ws) \cdot cP_w(Temp) + ws \cdot cPi(Temp, ws)$$

$$Mnacl := \frac{58.44277}{1000}$$

$$b := \left(Mnacl \cdot \left(\frac{1}{ws} - 1\right)\right)^{-1}$$

$$ksal(Temp, b) := \left(\left(0.5621 - 0.01394 \cdot b + 0.00177 \cdot b^2\right) + \left(0.00199 - 0.000294 \cdot b - 6.3 \cdot 10^{-5} \cdot b^2\right) \cdot Temp\right)$$

Para el tubo 1

$$D_{o1} = 0.019 \text{ m} \quad D_{in1} = 0.015 \text{ m} \quad P_{T1} = 0.024 \text{ m}$$

$$Temp_{proH} := \frac{Temp_{Hin} + Temp_{Hout}}{2} = 62.5 \quad Temp_{proHk} := Temp_{proH} + 273.2 = 335.7$$

$$Temp_{proC} := \frac{Temp_{Cin} + Temp_{Cout}}{2} = 25 \quad Temp_{proCk} := Temp_{proC} + 273.2 = 298.2$$

$$\delta_a := \delta_w(Temp_{proH}) = 981.905 \frac{kg}{m^3}$$

$$\delta_s := \delta_{sol}(ws, \delta_{ap}, Temp_{proC}) = (1.107 \cdot 10^3)$$

$$\mu_a := \mu_w(Temp_{proH}) = (4.495 \cdot 10^{-4}) \frac{kg}{m \cdot s}$$

$$\mu_s := \mu_{sol}(ws, Temp_{proC}) = 0.001201 \frac{kg}{m \cdot s}$$

$$cP_a := cP_w(Temp_{proH}) = (4.182 \cdot 10^3) \frac{m^2}{s^2}$$

$$cPsol(Temp, ws) := (1-ws) \cdot cP_w(Temp) + ws \cdot cPi(Temp, ws)$$

$$k_a := k_w (Temp_{proHk}) = 0.65 \frac{kg \cdot m}{s^3 \cdot K}$$

$$cP_s := cP_{sol} (Temp_{proC}, ws) = (3.557 \cdot 10^3)$$

$$k_s := k_{sal} (Temp_{proC}, b) = 0.542 \frac{kg \cdot m}{s^3 \cdot K}$$

Como se está diseñando se va a elegir un coeficiente global de diseño de tabla y luego se va a verificarlo - En la tabla no hay un valor para los fluidos que tenemos, entonces se extrae un valor de un paper específico

$$U_{gdiseño} := (600) \cdot \frac{W}{m^2 \cdot \Delta^\circ C} = 600 \frac{kg}{s^3 \cdot K}$$

$$q := (Q_{ms} \cdot cP_s \cdot (Temp_{Cout} - Temp_{Cin})) \cdot K$$

$$q = 607.612 \text{ kW}$$

Con el servicio y el U diseñado obtengo un área de diseño

Valores de prueba

$$Q_{ma} := 1 \frac{kg}{hr}$$

Solver Restricciones

$$q = (Q_{ma} \cdot cP_a \cdot (Temp_{Hin} - Temp_{Hout})) \cdot K$$

$$Q_{ma} := \text{find} (Q_{ma}) = (1.494 \cdot 10^4) \frac{kg}{hr}$$

$$LMTD_{ctc} := \left(\frac{(Temp_{Hout} - Temp_{Cin}) - (Temp_{Hin} - Temp_{Cout})}{\ln \left(\frac{(Temp_{Hout} - Temp_{Cin})}{(Temp_{Hin} - Temp_{Cout})} \right)} \right) \cdot \Delta^\circ C = 37.444 \text{ K}$$

$$\Delta T_{max} := (Temp_{Hin} - Temp_{Cin}) \cdot K = 70 \text{ K}$$

$$P := \frac{(Temp_{Cout} - Temp_{Cin}) \cdot K}{\Delta T_{max}}$$

$$C_p := cP_a \cdot Q_{ma} = (1.736 \cdot 10^4) \frac{kg \cdot m^2}{s^3 \cdot K}$$

$$C_C := cP_s \cdot Q_{ms} = (2.025 \cdot 10^4) \frac{\text{kg} \cdot \text{m}^2}{\text{s}^3 \cdot \text{K}}$$

$$R = \frac{C_C}{C_H} \quad R := \frac{(\text{Temp}_{Hin} - \text{Temp}_{Hout})}{(\text{Temp}_{Cout} - \text{Temp}_{Cin})} = 1.167$$

$$S := \frac{\sqrt{R^2 + 1}}{R - 1} = 9.22$$

$$W := \left(\frac{1 - P \cdot R}{1 - P} \right)^{\frac{1}{n_{ps}}} = 0.875$$

$$F_t := \frac{S \cdot \ln(W)}{\ln\left(\frac{1 + W - S + S \cdot W}{1 + W + S - S \cdot W}\right)} = 0.859$$

el valor es mayor a 0.75 así que es aceptable y no es necesario aumentar el número de pasos por coraza

$$A_{tdiseño} := \frac{q}{U_{gdiseño} \cdot LMTD_{ctc} \cdot F_t}$$

$A_{tdiseño} = 31.473 \text{ m}^2$ área que el equipo necesitaría

$$N_{t1} := \text{ceil}\left(\frac{A_{tdiseño}}{\pi \cdot D_{o1} \cdot L_t}\right) = 88 \quad N_{t2} := \text{ceil}\left(\frac{A_{tdiseño}}{\pi \cdot D_{o2} \cdot L_t}\right) = 66$$

Con el número de tubos se puede obtener el D de coraza D_s que también se pueden obtener de tabla

$$CTP := 0.9$$

$$CL := \frac{\sqrt[2]{3}}{2} = 0.866$$

$$D_{s1diseño} := \frac{2 \cdot P_{T1}}{\pi} \cdot \sqrt{\left(\frac{CL}{CTP}\right) \cdot \frac{A_{tdiseño}}{D_{o1} \cdot L_t}} \quad D_{s2diseño} := \frac{2 \cdot P_{T2}}{\pi} \cdot \sqrt{\left(\frac{CL}{CTP}\right) \cdot \frac{A_{tdiseño}}{D_{o2} \cdot L_t}}$$

$$D_{s1diseño} = 0.247 \text{ m}$$

$$D_{s2diseño} = 0.285 \text{ m}$$

De tabla se puede obtener el diámetro de coraza según tema

donde CTP
cobertura i
empaqueta
EL 90%

$$D_{s1dis} := 12 \text{ in} = 0.305 \text{ m} \quad D_{s2dis} := 13.25 \text{ in} = 0.337 \text{ m}$$

$$N_{t1} := 94 \quad N_{t2} := 62 \quad \text{escogidos de tabla, usando el criterio de elegir los más cercanos}$$

Cálculo del área de empaquetamiento y del diámetro mínimo de la coraza

$$A_{tube}(P_T) := P_T^2 \cdot CL$$

$$A_{bundle}(N_t, D_o, P_T) := 2 \cdot \left(\frac{N_t \cdot A_{tube}(P_T)}{\pi} \right)^{0.5} \cdot D_o \cdot (n_{pi} - 1) + N_t \cdot A_{tube}(P_T)$$

$$D_{smin}(N_t, D_o, P_T) := 2 \cdot \left(\frac{A_{bundle}(N_t, D_o, P_T)}{\pi} \right)^{0.5} + 2 \cdot D_o$$

$$A_{bundle1} := A_{bundle}(N_{t1}, D_{o1}, P_{T1}) = 0.051 \text{ m}^2 \quad A_{bundle2} := A_{bundle}(N_{t2}, D_{o2}, P_{T2}) = 0.061 \text{ m}^2$$

$$D_{smin1} := D_{smin}(N_{t1}, D_{o1}, P_{T1}) = 11.511 \text{ in} \quad D_{smin2} := D_{smin}(N_{t2}, D_{o2}, P_{T2}) = 12.954 \text{ in}$$

A partir de confirmar que el diámetro de coraza sea mayor que el diámetro mínimo necesario, y de tener el n° de tubos de tabla, se calcula el área disponible

$$A_{dispo}(N_t, D_o) := \pi \cdot D_o \cdot L_t \cdot N_t$$

$$A_{disp1} := A_{dispo}(N_{t1}, D_{o1}) = 33.754 \text{ m}^2$$

$$A_{disp2} := A_{dispo}(N_{t2}, D_{o2}) = 29.684 \text{ m}^2$$

Se proponen los diferentes espaciados y cortes y se verifica

$$A_{tp}(D_{in}, N_t) := \frac{\pi \cdot D_{in}^2}{4} \cdot N_t$$

$$G_i(D_{in}, N_t, Q_m) := \frac{Q_m \cdot 4 \cdot n_{pi}}{\pi \cdot D_{in}^2 \cdot N_t}$$

$$Rey_i(D_{in}, N_t, Q_m, \mu) := \frac{D_{in} \cdot G_i(D_{in}, N_t, Q_m)}{\mu}$$

$$Pr(u.k.cP) := \frac{cP \cdot \mu}{\mu}$$

$$B_1 := 0.2$$

$$c(P_T, D_o) :=$$

$$A_s(P_T, D_o,)$$

$$G_s(Q_m, P_T)$$

$$D_{eq\Delta}(P_T, L)$$

$$f(D_{in}, N_t, Q_m, \mu) := (1.821 \cdot \log(Rey_i(D_{in}, N_t, Q_m, \mu) - 1.64))^{-2}$$

$$Rey_s(Q_m, \mu)$$

$$Nu(D_{in}, N_t, Q_m, \mu, k, cP) := \frac{\left(\frac{f(D_{in}, N_t, Q_m, \mu)}{8} \right) \cdot (Rey_i(D_{in}, N_t, Q_m, \mu) - 1000) \cdot Pr(\mu, k, cP)}{1 + 12.7 \cdot \left(\frac{f(D_{in}, N_t, Q_m, \mu)}{8} \right)^{\frac{1}{2}} \cdot \left(Pr(\mu, k, cP)^{\frac{2}{3}} - 1 \right)}$$

$$f_{Di}(D_{in}, N_t, Q_m, \mu) := \frac{1}{\left(-2 \cdot \log \left(\frac{\frac{\varepsilon}{D_{in}}}{3.7065} - \frac{5.0452}{Rey_i(D_{in}, N_t, Q_m, \mu)} \cdot \log \left(\frac{1}{2.8257} \cdot \left(\frac{\varepsilon}{D_{in}} \right)^{1.1098} \right) \right) + \frac{5.8}{Rey_i(D_{in}, N_t, Q_m, \mu)}}}$$

$$\Delta P_i(D_{in}, N_t, Q_m, \mu, \delta) = f_{Di}(D_{in}, N_t, Q_m, \mu) \cdot n_{pi} \cdot \frac{L_t}{D_{in}} \cdot \frac{G_i(D_{in}, N_t, Q_m)^2}{2 \cdot \delta} \cdot \left(\frac{\mu}{\mu_{wall}} \right)^{-\gamma}$$

$$\Delta P_r(D_{in}, N_t, Q_m) = 4 \cdot n_{pi} \cdot \frac{G_i(D_{in}, N_t, Q_m)^2}{2 \cdot \delta}$$

$$\Delta P_{Ti}(D_{in}, N_t, Q_m, \mu, \delta) := \frac{G_i(D_{in}, N_t, Q_m)^2}{2 \cdot \delta} \cdot \left(f_{Di}(D_{in}, N_t, Q_m, \mu) \cdot n_{pi} \cdot \frac{L_t}{D_{in}} + 4 \cdot n_{pi} \right)$$

Cálculo de coeficientes peliculares para el tubo 1

$$Nu(D_{in1}, N_{t1}, Q_{ms}, \mu_s, k_s, cP_s) = 51.428$$

$$Nu_s(Q_{ma}, P_{T1}, D_{in1})$$

$$h_i(D_{in}, N_t, Q_m, \mu, k, cP) := \frac{Nu(D_{in}, N_t, Q_m, \mu, k, cP) \cdot k}{D_{in}}$$

$$h_o(Q_m, P_T, D_o, \mu, k, cP)$$

$$h_i(D_{in1}, N_{t1}, Q_{ms}, \mu_s, k_s, cP_s) = (1.88 \cdot 10^3) \frac{kg}{s^3 \cdot K}$$

$$h_{o11} := h_o(Q_{ma}, P_{T1}, D_{in1})$$

$$h_{io}(D_{in}, N_t, Q_m, \mu, k, cP, D_o) := h_i(D_{in}, N_t, Q_m, \mu, k, cP) \cdot \frac{D_{in}}{D_o}$$

$$h_{o12} := h_o(Q_{ma}, P_{T1}, D_{in1})$$

$$h_{io1} := h_{io}(D_{in1}, N_{t1}, Q_{ms}, \mu_s, k_s, cP_s, D_{o1}) = (1.464 \cdot 10^3) \frac{kg}{s^3 \cdot K}$$

$$h_{o13} := h_o(Q_{ma}, P_{T1}, D_{in1})$$

$$h_{o14} := h_o(Q_{ma}, P_{T1}, D_o)$$

$$U_g(h_{io}, h_o, D_o, D_{in}) := \left(\frac{1}{h_{io}} + \frac{1}{h_o} + R_{ad} + \frac{D_o}{2 \cdot k_{ac}} \cdot \ln \left(\frac{D_o}{D_{in}} \right) \right)^{-1}$$

$$U_{g11} := U_g(h_{io1}, h_{o11}, D_{o1}, D_{in1}) = 640.505 \frac{kg}{s^3 \cdot K}$$

$$U_{g13} := U_g(h_{io1}, h_{o13}, D_{o1}, D_{in1}) = 598.67 \frac{kg}{s^3 \cdot K}$$

$$U_{g12} := U_g(h_{io1}, h_{o12}, D_{o1}, D_{in1}) = 616.416 \frac{kg}{s^3 \cdot K}$$

$$U_{g14} := U_g(h_{io1}, h_{o14}, D_{o1}, D_{in1}) = 584.245 \frac{kg}{s^3 \cdot K}$$

$$A_{tdisp}(h_{io}, h_o, D_o, D_{in}) := \frac{q}{U_g(h_{io}, h_o, D_o, D_{in}) \cdot LMTD_{ctc} \cdot F_t}$$

En realidad es área necesaria o requerida, me olvidé cambiar el nombre cuando copié la ecuación

$$A_{t11} := A_{tdisp}(h_{io1}, h_{o11}, D_{o1}, D_{in1}) = 29.483 m^2$$

$$A_{t13} := A_{tdisp}(h_{io1}, h_{o13}, D_{o1}, D_{in1}) = 31.543 m^2$$

$$A_{t12} := A_{tdisp}(h_{io1}, h_{o12}, D_{o1}, D_{in1}) = 30.635 m^2$$

$$A_{t14} := A_{tdisp}(h_{io1}, h_{o14}, D_{o1}, D_{in1}) = 32.322 m^2$$

$$\Delta P_{Ti1} := \Delta P_{Ti}(D_{in1}, N_{t1}, Q_{ms}, \mu_s, \delta_s) = 7.583 kPa$$

$$\Delta P_{s11} := \Delta P_s(Q_{ma}, P_{T1}, D_o)$$

$$\Delta P_{s12} := \Delta P_s(Q_{ma}, P_{T1}, D_o)$$

$$\Delta P_{s13} := \Delta P_s(Q_{ma}, P_{T1}, D_o)$$

$$\Delta P_{s14} := \Delta P_s(Q_{ma}, P_{T1}, D_o)$$

Cálculo de coeficientes peliculares para el tubo 2

$$Nu(D_{in2}, N_{t2}, Q_{ms}, \mu_s, k_s, cP_s) = 54.522$$

$$Nu_s(Q_{ma}, P_{T2}, D_o)$$

$$h_i(D_{in}, N_t, Q_m, \mu, k, cP) := \frac{Nu(D_{in}, N_t, Q_m, \mu, k, cP) \cdot k}{D_{in}}$$

$$h_o(Q_m, P_T, D_o, L)$$

$$h_i(D_{in}, N_t, Q_m, \mu, k, cP) = (1.396 \cdot 10^3) \frac{kg}{s^3 \cdot K}$$

$$h_o(Q_m, P_T, D_o, L)$$

$$s^3 \cdot K$$

$$h_{io}(D_{in}, N_t, Q_m, \mu, k, cP, D_o) := h_i(D_{in}, N_t, Q_m, \mu, k, cP) \cdot \frac{D_{in}}{D_o}$$

$$h_{o22} := h_o(Q_{ma}, P_{T2}, L_{c2})$$

$$h_{io2} := h_{io}(D_{in2}, N_{t2}, Q_{ms}, \mu_s, k_s, cP_s, D_{o2}) = (1.164 \cdot 10^3) \frac{kg}{s^3 \cdot K}$$

$$h_{o23} := h_o(Q_{ma}, P_{T2}, L_{c3})$$

$$h_{o24} := h_o(Q_{ma}, P_{T2}, L_{c4})$$

$$U_g(h_{io}, h_o, D_o, D_{in}) := \left(\frac{1}{h_{io}} + \frac{1}{h_o} + R_{ad} + \frac{D_o}{2 \cdot k_{ac}} \cdot \ln \left(\frac{D_o}{D_{in}} \right) \right)^{-1}$$

$$U_{g21} := U_g(h_{io2}, h_{o21}, D_{o2}, D_{in2}) = 565.632 \frac{kg}{s^3 \cdot K}$$

$$U_{g23} := U_g(h_{io2}, h_{o23}, D_{o2}, D_{in2}) = 524.545 \frac{kg}{s^3 \cdot K}$$

$$U_{g22} := U_g(h_{io2}, h_{o22}, D_{o2}, D_{in2}) = 541.895 \frac{kg}{s^3 \cdot K}$$

$$U_{g24} := U_g(h_{io2}, h_{o24}, D_{o2}, D_{in2}) = 510.527 \frac{kg}{s^3 \cdot K}$$

$$A_{tdisp}(h_{io}, h_o, D_o, D_{in}) := \frac{q}{U_g(h_{io}, h_o, D_o, D_{in}) \cdot LMTD_{cte} \cdot F_t}$$

$$A_{t21} := A_{tdisp}(h_{io2}, h_{o21}, D_{o2}, D_{in2}) = 33.386 m^2$$

$$A_{t23} := A_{tdisp}(h_{io2}, h_{o23}, D_{o2}, D_{in2}) = 36.001 m^2$$

$$A_{t22} := A_{tdisp}(h_{io2}, h_{o22}, D_{o2}, D_{in2}) = 34.848 m^2$$

$$A_{t24} := A_{tdisp}(h_{io2}, h_{o24}, D_{o2}, D_{in2}) = 36.001 m^2$$

$$\Delta P_{Ti2} := \Delta P_{Ti}(D_{in2}, N_{t2}, Q_{ms}, \mu_s, \delta_s) = 3.189 kPa$$

$$\Delta P_{s21} := \Delta P_s(Q_{ma}, P_{T2}, L_{c1})$$

$$\Delta P_{s22} := \Delta P_s(Q_{ma}, P_{T2}, L_{c2})$$

$$\Delta P_{s23} := \Delta P_s(Q_{ma}, P_{T2}, L_{c3})$$

$$\Delta P_{s24} := \Delta P_s(Q_{ma}, P_{T2}, L_{c4})$$

INCISO b método Delaware- dimensionamiento

sólo delaware indica que el corte y el espaciado de

$$P_{Tef}(P_T) := P_T \cdot CL$$

$$L_{c1} := 0.15$$

$$L_{c2} := 0.20$$

$$L_{c3} := 0.25$$

$$L_{c4} := 0.30$$

$$J_l := 0.75 \quad J_b := 0.80 \quad J_s := 0.925$$

$$a := 0.249 \quad b := 2.207$$

$$D_{bdl}(D_o, N_t) := D_o \cdot \left(\frac{N_t}{a} \right)^{\frac{1}{b}}$$

$$\phi(D_o, N_t, D_s, L_c) := \frac{(D_s - 2 \cdot L_c \cdot D_s)}{D_{bdl}(D_o, N_t)}$$

$$\theta(D_o, N_t, D_s, L_c) := 2 \cdot \arccos(\phi(D_o, N_t, D_s, L_c))$$

$$F_c(D_o, N_t, D_s, L_c) := \frac{1}{\pi} \cdot \left(\pi + 2 \cdot \phi(D_o, N_t, D_s, L_c) \cdot \sin\left(\frac{\theta(D_o, N_t, D_s, L_c)}{2}\right) - \theta(D_o, N_t, D_s, L_c) \right)$$

$$J_c(D_o, N_t, D_s, L_c) := 0.55 + 0.72 \cdot F_c(D_o, N_t, D_s, L_c)$$

$$J_c(D_{o1}, N_{t1}, D_{s1dis}, L_{c1}) \cdot J_l \cdot J_b \cdot J_s = 0.651$$

$$A_{sD}(D_s, P_T, N_t, D_o, B) := B \cdot D_s \cdot \left((D_s - D_{bdl}(D_o, N_t)) + \frac{(D_{bdl}(D_o, N_t) - D_o)}{P_{Tef}(P_T)} \cdot (P_T - D_o) \right)$$

$$G_{sD}(D_s, P_T, N_t, D_o, B) := \frac{Q_{ma}}{A_{sD}(D_s, P_T, N_t, D_o, B)}$$

$$Pr(\mu, k, cP) := \frac{cP \cdot \mu}{k}$$

$$Rey_s(D_o, D_s, P_T, N_t, \mu, B) := \frac{D_o \cdot G_{sD}(D_s, P_T, N_t, D_o, B)}{\mu}$$

Para el tubo 1

$$Rey_{11} := Rey_s(D_{o1}, D_{s1dis}, P_{T1}, N_{t1}, \mu_a, B_1) = 3.4 \cdot 10^4$$

$$Rey_{12} := Rey_s(D_{o1}, D_{s1dis}, P_{T1}, N_{t1}, \mu_a, B_2) = 1.7 \cdot 10^4$$

$$Rey_{13} := Rey_s(D_{o1}, D_{s1dis}, P_{T1}, N_{t1}, \mu_a, B_3) = 1.133 \cdot 10^4$$

$$Rey_{14} := Rey_s(D_{o1}, D_{s1dis}, P_{T1}, N_{t1}, \mu_a, B_4) = 8.499 \cdot 10^3$$

El Reynolds está entre 10 a la cuarta y al cubo, se escoge un layout angle de 30°: por lo que se escogen las constantes:

$$a_1 := 0.321 \quad a_2 := -0.388 \quad a_3 := 1.450 \quad a_4 := 0.519 \quad b_1 := 0.486 \quad b_2 := -0.152$$

Triangula
Square pi
Pitch = 1.2

Compa

Cómputo de P

$J_{id} = a_1$

Layout Angle

30°

45°

90°

$$b_3 := 7 \quad b_4 := 0.5$$

$$a(D_o, D_s, P_T, N_t, \mu, B) := \frac{a_3}{1 + 0.14 \cdot \text{Rey}_s(D_o, D_s, P_T, N_t, \mu, B)^{a_4}}$$

$$j_{id}(D_o, D_s, P_T, N_t, \mu, B) := a_1 \cdot \left(\frac{1.33 \cdot D_o}{P_T} \right)^{a(D_o, D_s, P_T, N_t, \mu, B)} \cdot \text{Rey}_s(D_o, D_s, P_T, N_t, \mu, B)^{a_2}$$

$$h_{id}(D_s, P_T, N_t, \mu, k, cP, D_o, B) = j_{id}(D_o, D_s, P_T, N_t, \mu, B) \cdot cP \cdot G_{sD}(D_s, P_T, N_t, D_o, B) \cdot Pr(\mu, k, cP)^{\frac{-2}{3}}$$

$$h_{id}(D_s, P_T, N_t, \mu, k, cP, D_o, B) := j_{id}(D_o, D_s, P_T, N_t, \mu, B) \cdot cP \cdot G_{sD}(D_s, P_T, N_t, D_o, B) \cdot Pr(\mu, k, cP)^{\frac{-2}{3}}$$

$$h_s(D_s, P_T, N_t, \mu, k, cP, D_o, B, L_c) := h_{id}(D_s, P_T, N_t, \mu, k, cP, D_o, B) \cdot J_c(D_o, N_t, D_s, L_c) \cdot J_l \cdot J_b \cdot J_s$$

$$h_{s11} := h_s(D_{s1dis}, P_{T1}, N_{t1}, \mu_a, k_a, cP_a, D_{o1}, B_1, L_{c1}) = (6.044 \cdot 10^3) \frac{\text{kg}}{\text{s}^3 \cdot \text{K}} \quad h_{s13} := h_s(D_{s1dis}, P_{T1}, N_{t1}, \mu_a, k_a, cP_a, D_{o1}, B_1, L_{c1}) = (6.044 \cdot 10^3) \frac{\text{kg}}{\text{s}^3 \cdot \text{K}}$$

$$h_{s12} := h_s(D_{s1dis}, P_{T1}, N_{t1}, \mu_a, k_a, cP_a, D_{o1}, B_2, L_{c2}) = (3.721 \cdot 10^3) \frac{\text{kg}}{\text{s}^3 \cdot \text{K}} \quad h_{s14} := h_s(D_{s1dis}, P_{T1}, N_{t1}, \mu_a, k_a, cP_a, D_{o1}, B_2, L_{c2}) = (3.721 \cdot 10^3) \frac{\text{kg}}{\text{s}^3 \cdot \text{K}}$$

$$U_g(h_{io}, h_s, D_o, D_{in}) := \left(\frac{1}{h_{io}} + \frac{1}{h_s} + R_{ad} + \frac{D_o}{2 \cdot k_{ac}} \cdot \ln \left(\frac{D_o}{D_{in}} \right) \right)^{-1}$$

$$U_{g11} := U_g(h_{io1}, h_{s11}, D_{o1}, D_{in1}) = 626.86 \frac{\text{kg}}{\text{s}^3 \cdot \text{K}} \quad U_{g13} := U_g(h_{io1}, h_{s13}, D_{o1}, D_{in1}) = 555.327 \frac{\text{kg}}{\text{s}^3 \cdot \text{K}}$$

$$U_{g12} := U_g(h_{io1}, h_{s12}, D_{o1}, D_{in1}) = 588.752 \frac{\text{kg}}{\text{s}^3 \cdot \text{K}} \quad U_{g14} := U_g(h_{io1}, h_{s14}, D_{o1}, D_{in1}) = 522.776 \frac{\text{kg}}{\text{s}^3 \cdot \text{K}}$$

$$A_{tdisp}(h_{io}, h_s, D_o, D_{in}) := \frac{q}{U_g(h_{io}, h_s, D_o, D_{in}) \cdot \text{LMTD}_{ctc} \cdot F_t}$$

$$A_{t11} := A_{tdisp}(h_{io1}, h_{s11}, D_{o1}, D_{in1}) = 30.125 \text{ m}^2$$

$$A_{t13} := A_{tdisp}(h_{io1}, h_{s13}, D_{o1}, D_{in1}) = 34.005 \text{ m}^2$$

$$A_{t12} := A_{tdisp}(h_{io1}, h_{s12}, D_{o1}, D_{in1}) = 32.075 \text{ m}^2$$

$$A_{t14} := A_{tdisp}(h_{io1}, h_{s14}, D_{o1}, D_{in1}) = 36.123 \text{ m}^2$$

$$\Delta P_{Ti1} := \Delta P_{Ti}(D_{in1}, N_{t1}, Q_{ms}, \mu_s, \delta_s) = 7.583 \text{ kPa}$$

Caída de presión en la coraza

$$L_{c1} := 0.15 \quad L_{c2} := 0.20 \quad L_{c3} := 0.25 \quad L_{c4} := 0.30$$

$$\phi(D_o, N_t, D_s, L_c) := \frac{(D_s - 2 \cdot L_c \cdot D_s)}{D_{bdl}(D_o, N_t)}$$

$$\theta(D_o, N_t, D_s, L_c) := 2 \cdot \arccos(\phi(D_o, N_t, D_s, L_c))$$

$$F_{tw}(D_o, N_t, D_s, L_c) := \frac{\theta(D_o, N_t, D_s, L_c) - \sin(\theta(D_o, N_t, D_s, L_c))}{2 \cdot \pi}$$

$$N_{tw}(D_o, N_t, D_s, L_c) := F_{tw}(D_o, N_t, D_s, L_c) \cdot N_t$$

$$A_{wt}(D_o, N_t, D_s, L_c) := N_{tw}(D_o, N_t, D_s, L_c) \cdot \frac{\pi \cdot D_o^2}{4}$$

$$A_{wg}(D_o, N_t, D_s, L_c) := \frac{\pi \cdot D_s^2}{8} \cdot \theta(D_o, N_t, D_s, L_c) - \sin\left(\frac{\theta(D_o, N_t, D_s, L_c)}{2}\right) \cdot \left(\frac{D_s}{2}\right) \cdot \left(\frac{D_s}{2} - L_c \cdot D_s\right)$$

$$A_{win}(D_o, N_t, D_s, L_c) := A_{wg}(D_o, N_t, D_s, L_c) - A_{wt}(D_o, N_t, D_s, L_c)$$

$$R_l := 0.45 \quad R_b := 0.65$$

Rl: corrección por fuga en deflector
Rb: corrección por bypass

$$N_{cw}(P_T, D_s, L_c) := \frac{0.8 \cdot L_c \cdot D_s}{P_{Tef}(P_T)}$$

$$N_B(B, D_s) := \frac{L_t}{B \cdot D_s} - 1$$

Ncw n° efect de tubos en ca
ventana

$$\Delta P_{wind}(D_s, P_T, N_t, D_o, B, L_c, Q_m, \delta) := n_{ps} \cdot \left(\frac{Q_m^2 \cdot (2 + 0.6 \cdot N_{cw}(P_T, D_s, L_c))}{2 \cdot \delta \cdot A_{sD}(D_s, P_T, N_t, D_o, B) \cdot A_{win}(D_o, N_t, D_s, L_c)} \right) \cdot N_B(B, D_s)$$

$$b(D_o, D_s, P_T, N_t, \mu, B) := \frac{b_3}{1 + 0.14 \cdot Re_{ys}(D_o, D_s, P_T, N_t, \mu, B)^{b_4}}$$

$$f_{id}(D_o, D_s, P_T, N_t, \mu, B) := b_1 \cdot \left(\frac{1.33 \cdot D_o}{P_T} \right)^{b(D_o, D_s, P_T, N_t, \mu, B)} \cdot \text{Rey}_s(D_o, D_s, P_T, N_t, \mu, B)^{b_2}$$

$$\Delta P_{bi} = n_{ps} \cdot 4 \cdot f_{id}(D_o, D_s, P_T, N_t, \mu, B) \cdot \frac{G_{sD}(D_s, P_T, N_t, D_o, B)^2}{2 \cdot \delta} \cdot \left(\frac{\mu}{\mu_{wall}} \right)^{-0.14}$$

$$\Delta P_{bi}(D_o, D_s, P_T, N_t, \mu, B, \delta) := n_{ps} \cdot 4 \cdot f_{id}(D_o, D_s, P_T, N_t, \mu, B) \cdot \frac{G_{sD}(D_s, P_T, N_t, D_o, B)^2}{2 \cdot \delta}$$

$$\Delta P_{cf}(D_o, D_s, P_T, N_t, \mu, B, \delta) := \Delta P_{bi}(D_o, D_s, P_T, N_t, \mu, B, \delta) \cdot (N_B(B, D_s) - 1) \cdot R_l \cdot R_b$$

$$\Delta P_s(D_o, D_s, P_T, N_t, \mu, B, \delta, L_c, Q_m) := \Delta P_{cf}(D_o, D_s, P_T, N_t, \mu, B, \delta) + \Delta P_{wind}(D_s, P_T, N_t, D_o, B, L_c, Q_m)$$

$$\Delta P_{s11} := \Delta P_s(D_{o1}, D_{s1dis}, P_{T1}, N_{t1}, \mu_a, B_1, \delta_a, L_{c1}, Q_{ma}) = 9.562 \text{ kPa}$$

$$\Delta P_{s12} := \Delta P_s(D_{o1}, D_{s1dis}, P_{T1}, N_{t1}, \mu_a, B_2, \delta_a, L_{c2}, Q_{ma}) = 1.794 \text{ kPa}$$

$$\Delta P_{s13} := \Delta P_s(D_{o1}, D_{s1dis}, P_{T1}, N_{t1}, \mu_a, B_3, \delta_a, L_{c3}, Q_{ma}) = 0.682 \text{ kPa}$$

$$\Delta P_{s14} := \Delta P_s(D_{o1}, D_{s1dis}, P_{T1}, N_{t1}, \mu_a, B_4, \delta_a, L_{c4}, Q_{ma}) = 0.345 \text{ kPa}$$

tubo 2

$$h_{s21} := h_s(D_{s2dis}, P_{T2}, N_{t2}, \mu_a, k_a, cP_a, D_{o2}, B_1, L_{c1}) = (4.819 \cdot 10^3) \frac{\text{kg}}{\text{s}^3 \cdot \text{K}} \quad h_{s23} := h_s(D_{s2dis}, P_{T2}, N_{t2}, \mu_a, k_a, cP_a, D_{o2}, B_1, L_{c1}) = (4.819 \cdot 10^3) \frac{\text{kg}}{\text{s}^3 \cdot \text{K}}$$

$$h_{s22} := h_s(D_{s2dis}, P_{T2}, N_{t2}, \mu_a, k_a, cP_a, D_{o2}, B_2, L_{c2}) = (2.967 \cdot 10^3) \frac{\text{kg}}{\text{s}^3 \cdot \text{K}} \quad h_{s24} := h_s(D_{s2dis}, P_{T2}, N_{t2}, \mu_a, k_a, cP_a, D_{o2}, B_2, L_{c2}) = (2.967 \cdot 10^3) \frac{\text{kg}}{\text{s}^3 \cdot \text{K}}$$

$$U_g(h_{io}, h_s, D_o, D_{in}) := \left(\frac{1}{h_{io}} + \frac{1}{h_s} + R_{ad} + \frac{D_o}{2 \cdot k_{ac}} \cdot \ln \left(\frac{D_o}{D_{in}} \right) \right)^{-1}$$

$$U_{g21} := U_g(h_{io2}, h_{s21}, D_{o2}, D_{in2}) = 552.929 \frac{\text{kg}}{\text{s}^3 \cdot \text{K}} \quad U_{g23} := U_g(h_{io2}, h_{s23}, D_{o2}, D_{in2}) = 483.959 \frac{\text{kg}}{\text{s}^3 \cdot \text{K}}$$

$$U_{g22} := U_g(h_{io2}, h_{s22}, D_{o2}, D_{in2}) = 515.98 \frac{\text{kg}}{\text{s}^3 \cdot \text{K}}$$

$$U_{g24} := U_g(h_{io2}, h_{s24}, D_{o2}, D_{in2}) = 453.117 \frac{\text{kg}}{\text{s}^3 \cdot \text{K}}$$

$$A_{tdisp}(h_{io}, h_s, D_o, D_{in}) := \frac{q}{U_g(h_{io}, h_s, D_o, D_{in}) \cdot LMTD_{ctc} \cdot F_t}$$

$$A_{t21} := A_{tdisp}(h_{io2}, h_{s21}, D_{o2}, D_{in2}) = 34.153 \text{ m}^2$$

$$A_{t23} := A_{tdisp}(h_{io2}, h_{s23}, D_{o2}, D_{in2}) = 39.02 \text{ m}^2$$

$$A_{t22} := A_{tdisp}(h_{io2}, h_{s22}, D_{o2}, D_{in2}) = 36.598 \text{ m}^2$$

$$A_{t24} := A_{tdisp}(h_{io2}, h_{s24}, D_{o2}, D_{in2}) = 41.676 \text{ m}^2$$

$$\Delta P_{Ti2} := \Delta P_{Ti}(D_{in2}, N_{t2}, Q_{ms}, \mu_s, \delta_s) = 3.189 \text{ kPa}$$

$$\Delta P_s(D_o, D_s, P_T, N_t, \mu, B, \delta, L_c, Q_m) := \Delta P_{cf}(D_o, D_s, P_T, N_t, \mu, B, \delta) + \Delta P_{wind}(D_s, P_T, N_t, D_o, B, L_c, Q_m)$$

$$\Delta P_{s21} := \Delta P_s(D_{o2}, D_{s2dis}, P_{T2}, N_{t2}, \mu_a, B_1, \delta_a, L_{c1}, Q_{ma}) = 5.65 \text{ kPa}$$

$$\Delta P_{s22} := \Delta P_s(D_{o2}, D_{s2dis}, P_{T2}, N_{t2}, \mu_a, B_2, \delta_a, L_{c2}, Q_{ma}) = 1.042 \text{ kPa}$$

$$\Delta P_{s23} := \Delta P_s(D_{o2}, D_{s2dis}, P_{T2}, N_{t2}, \mu_a, B_3, \delta_a, L_{c3}, Q_{ma}) = 0.391 \text{ kPa}$$

$$\Delta P_{s24} := \Delta P_s(D_{o2}, D_{s2dis}, P_{T2}, N_{t2}, \mu_a, B_4, \delta_a, L_{c4}, Q_{ma}) = 0.196 \text{ kPa}$$

$$\Delta P_T(\Delta P_{Ti}, \Delta P_s) := \Delta P_{Ti} + \Delta P_s$$

COSTO

$$i := 0.03 \quad n := 10$$

$$a := \left(\frac{i \cdot (1+i)^n}{(1+i)^n - 1} \right) \frac{1}{yr} = 0.117 \frac{1}{yr}$$

Donde

i: interés

n: vida útil

a: amortización, en éste caso es a 10 años (vida útil)

Costo de la energía por bombeo

$$C_{ener} := \left(\frac{0.15}{1000 \cdot 3600} \right) \frac{\square}{J} = (4.167 \cdot 10^{-8}) \frac{\square}{J}$$

$$t := 335 \frac{\text{day}}{\text{yr}} \cdot 24 \frac{\text{hr}}{\text{day}} = (8.04 \cdot 10^3) \frac{\text{hr}}{\text{yr}}$$

cOSTO FIJO- COSTO DEL INTERCAMBIADOR (lo que se paga ahora)

$$C_{fijo}(A_t) := 1000 \cdot A_t \cdot 0.8 \frac{\square}{m^2} \quad \text{donde } A_t \text{ es el \u00e1rea requerida del intercambiador}$$

$$C_{fi11} := C_{fijo}(A_{t11}) = 24099.85 \square \quad C_{fi12} := C_{fijo}(A_{t12}) = 25659.765 \square$$

Para el tubo 1

$$C_{fi13} := C_{fijo}(A_{t13}) = 27204.211 \square \quad C_{fi14} := C_{fijo}(A_{t14}) = 28898.108 \square$$

$$C_{fi21} := C_{fijo}(A_{t21}) = 27322.206 \square \quad C_{fi22} := C_{fijo}(A_{t22}) = 29278.727 \square$$

Para el tubo 2

$$C_{fi23} := C_{fijo}(A_{t23}) = 31215.956 \square \quad C_{fi24} := C_{fijo}(A_{t24}) = 33340.714 \square$$

Costo amortizado, lo que voy a pagar en 10 a\u00f1os

$$C_{amor}(C_{fi}) := C_{fi} \cdot a$$

$$C_{am11} := C_{amor}(C_{fi11}) = 2825.238 \frac{\square}{\text{yr}} \quad C_{am13} := C_{amor}(C_{fi13}) = 3189.163 \frac{\square}{\text{yr}}$$

Para el tubo 1

$$C_{am12} := C_{amor}(C_{fi12}) = 3008.107 \frac{\square}{\text{yr}} \quad C_{am14} := C_{amor}(C_{fi14}) = 3387.74 \frac{\square}{\text{yr}}$$

$$C_{am21} := C_{amor}(C_{fi21}) = 3202.996 \frac{\square}{\text{yr}} \quad C_{am23} := C_{amor}(C_{fi23}) = 3659.462 \frac{\square}{\text{yr}}$$

Para el tubo 2

$$C_{am22} := C_{amor}(C_{fi22}) = 3432.36 \frac{\square}{\text{yr}} \quad C_{am24} := C_{amor}(C_{fi24}) = 3908.549 \frac{\square}{\text{yr}}$$

Costo de la potencia para el bombeo

$$Pot(\Delta P_s, \Delta P_{Ti}) := \Delta P_s \cdot \frac{Q_{ma}}{\delta_a \cdot 0.8} + \Delta P_{Ti} \cdot \frac{Q_{ms}}{\delta_s \cdot 0.8}$$

Cada t\u00e9rmino corresponde a la potencia de una bomba diferente porque son fluidos diferentes

$$C_{bomb}(\Delta P_s, \Delta P_{Ti}) := C_{ener} \cdot Pot(\Delta P_s, \Delta P_{Ti})$$

$$C_{bomb11} := C_{bomb}(\Delta P_{s11}, \Delta P_{Ti1}) = 130.579 \frac{\text{€}}{\text{yr}}$$

$$C_{bomb12} := C_{bomb}(\Delta P_{s12}, \Delta P_{Ti1}) = 76.596 \frac{\text{€}}{\text{yr}}$$

$$C_{bomb13} := C_{bomb}(\Delta P_{s13}, \Delta P_{Ti1}) = 68.871 \frac{\text{€}}{\text{yr}}$$

$$C_{bomb14} := C_{bomb}(\Delta P_{s14}, \Delta P_{Ti1}) = 66.531 \frac{\text{€}}{\text{yr}}$$

$$C_{bomb21} := C_{bomb}(\Delta P_{s21}, \Delta P_{Ti2}) = 66.227 \frac{\text{€}}{\text{yr}}$$

$$C_{bomb22} := C_{bomb}(\Delta P_{s22}, \Delta P_{Ti2}) = 28.329 \frac{\text{€}}{\text{yr}}$$

$$C_{bomb23} := C_{bomb}(\Delta P_{s23}, \Delta P_{Ti2}) = 29.686 \frac{\text{€}}{\text{yr}}$$

$$C_{bomb24} := C_{bomb}(\Delta P_{s24}, \Delta P_{Ti2}) = 50.93 \frac{\text{€}}{\text{yr}}$$

Costo total

$$C_T(C_{bomb}, C_{am}) := C_{bomb} + C_{am}$$

$$C_{T11} := C_T(C_{bomb11}, C_{am11}) = 2955.817 \frac{\text{€}}{\text{yr}}$$

$$C_{T12} := C_T(C_{bomb12}, C_{am12}) = 3084.703 \frac{\text{€}}{\text{yr}}$$

$$C_{T13} := C_T(C_{bomb13}, C_{am13}) = 3258.035 \frac{\text{€}}{\text{yr}}$$

$$C_{T14} := C_T(C_{bomb14}, C_{am14}) = 3454.27 \frac{\text{€}}{\text{yr}}$$

$$C_{T21} := C_T(C_{bomb21}, C_{am21}) = 3269.223 \frac{\text{€}}{\text{yr}}$$

$$C_{T22} := C_T(C_{bomb22}, C_{am22}) = 3460.689 \frac{\text{€}}{\text{yr}}$$

$$C_{T23} := C_T(C_{bomb23}, C_{am23}) = 3689.149 \frac{\text{€}}{\text{yr}}$$

$$C_{T24} := C_T(C_{bomb24}, C_{am24}) = 3959.479 \frac{\text{€}}{\text{yr}}$$

$$B_{t1} := \begin{bmatrix} B_1 \\ B_2 \\ B_3 \\ B_4 \end{bmatrix} \cdot D_{s1dis}$$

$$B_{t2} := \begin{bmatrix} B_1 \\ B_2 \\ B_3 \\ B_4 \end{bmatrix} \cdot D_{s2dis}$$

$$L_{ct1} := \begin{bmatrix} L_{c1} \\ L_{c2} \\ L_{c3} \\ L_{c4} \end{bmatrix} \cdot D_{s1dis}$$

$$L_{ct2} := \begin{bmatrix} L_{c1} \\ L_{c2} \\ L_{c3} \\ L_{c4} \end{bmatrix} \cdot D_{s2dis}$$

$$C_{T1} := \begin{bmatrix} C_{T11} \\ C_{T12} \\ C_{T13} \\ C_{T14} \end{bmatrix}$$

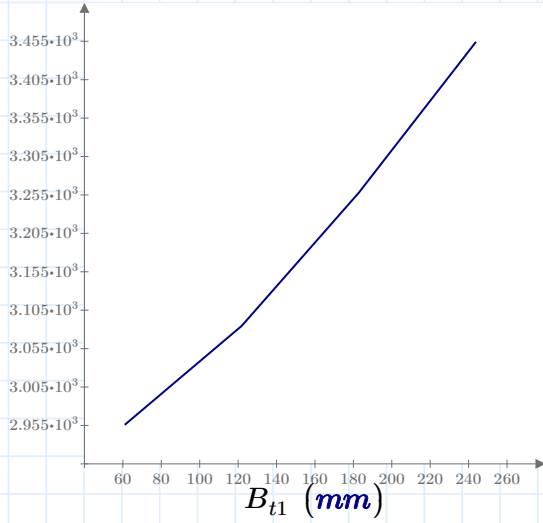
$$C_{T2} := \begin{bmatrix} C_{T21} \\ C_{T22} \\ C_{T23} \\ C_{T24} \end{bmatrix}$$

$$A_{t11} := A_{tdisp}(h_{io1}, h_{s11}, D_{o1}, D_{in1}) = 30.125 \text{ m}^2$$

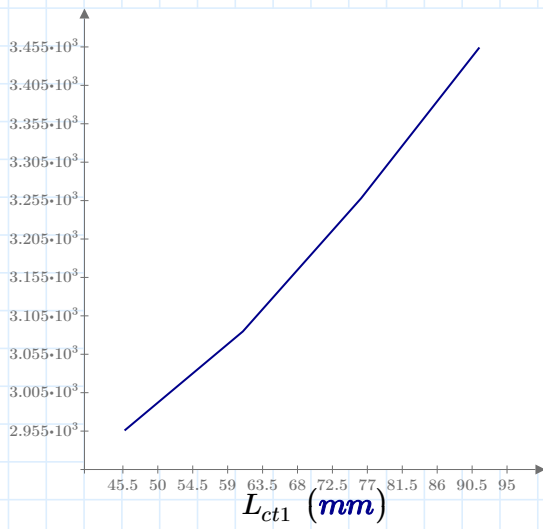
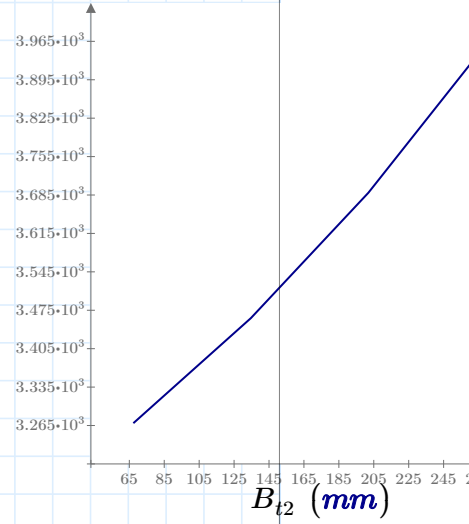
$$A_{t12} := A_{tdisp}(h_{io1}, h_{s12}, D_{o1}, D_{in1}) = 32.075 \text{ m}^2$$

$$A_{t21} := A_{tdisp}(h_{io2}, h_{s21}, D_{o2}, D_{in2}) = 34.153 \text{ m}^2$$

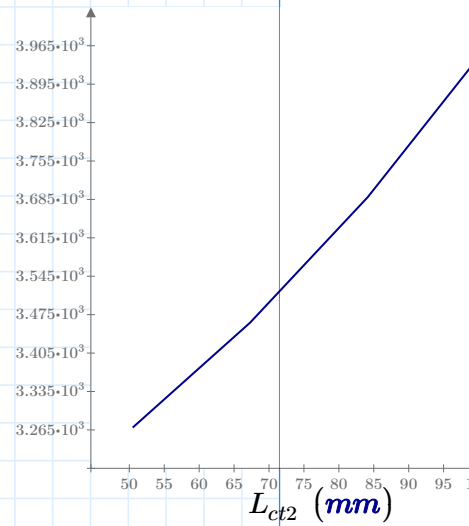
$$A_{t22} := A_{tdisp}(h_{io2}, h_{s22}, D_{o2}, D_{in2}) = 36.598 \text{ m}^2$$



$$C_{T1} \left(\frac{\text{yr}}{\text{yr}} \right)$$



$$C_{T1} \left(\frac{\text{yr}}{\text{yr}} \right)$$



VIDA ÚTIL

Cálculo de coeficiente global disponible

$$U_{disp1} := \frac{q}{A_{disp1} \cdot F_t \cdot LMTD_{ctc}} = 559.463 \frac{\text{kg}}{\text{s}^3 \cdot \text{K}}$$

$$U_{disp2} := \frac{q}{A_{disp2} \cdot F_t \cdot LMTD_{ctc}} = 636.163 \frac{\text{kg}}{\text{s}^3 \cdot \text{K}}$$

Cálculo de Rd disponible o calculado

$$R_{d1}(U_g) := \left(\frac{1}{U_{disp1}} - \frac{1}{U_g} \right)$$

$$R_{d11} := R_{d1}(U_{g11}) = (1.922 \cdot 10^{-4}) \frac{s^3 \cdot K}{kg}$$

$$R_{d12} := R_{d1}(U_{g12}) = (8.892 \cdot 10^{-5}) \frac{s^3 \cdot K}{kg}$$

$$R_{d13} := R_{d1}(U_{g13}) = -1.331 \cdot 10^{-5} \frac{s^3 \cdot K}{kg}$$

$$R_{d14} := R_{d1}(U_{g14}) = -1.254 \cdot 10^{-4} \frac{s^3 \cdot K}{kg}$$

$$R_{dT1} := \left(0.0005 \frac{m^2 \cdot \Delta^\circ C}{W} \cdot \frac{D_{o1}}{D_{in1}} + 0.0001 \frac{m^2 \cdot \Delta^\circ C}{W} \right) = (7.423 \cdot 10^{-4}) \frac{s^3 \cdot K}{kg}$$

Cálculo de la vida Útil

$$VU_1(R_{d1}) := \frac{R_{d1}}{R_{dT1}} \cdot 12$$

$$VU_1(R_{d11}) = 3.107 \quad VU_1(R_{d12}) = 1.438$$

$$VU_1(R_{d13}) = -0.215 \quad VU_1(R_{d14}) = -2.028$$

Que la vida útil de negativa, es indicativo de que el coeficiente global requerido es mayor al disponible, por lo que el área requerida es mayor a la disponible
 Con respecto a la vida útil, el intercambiador que habría que elegir es el de At12 porque su vida útil sobrepasa a 1 año de uso, luego de eso hay que limpiarlo, pero no está muy sobredimensionado como el de At11